



# GAS SYSTEM REPORT

AMS  
TRD MEETING  
Rome 19-20 October 2005



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# Engineering Box S Status

- USCM & can-box from Rome connected  
(no cables for MIT's)
- Dallas sensors: direct connection to USCM
- Gas bottles: Ar used instead of Xe

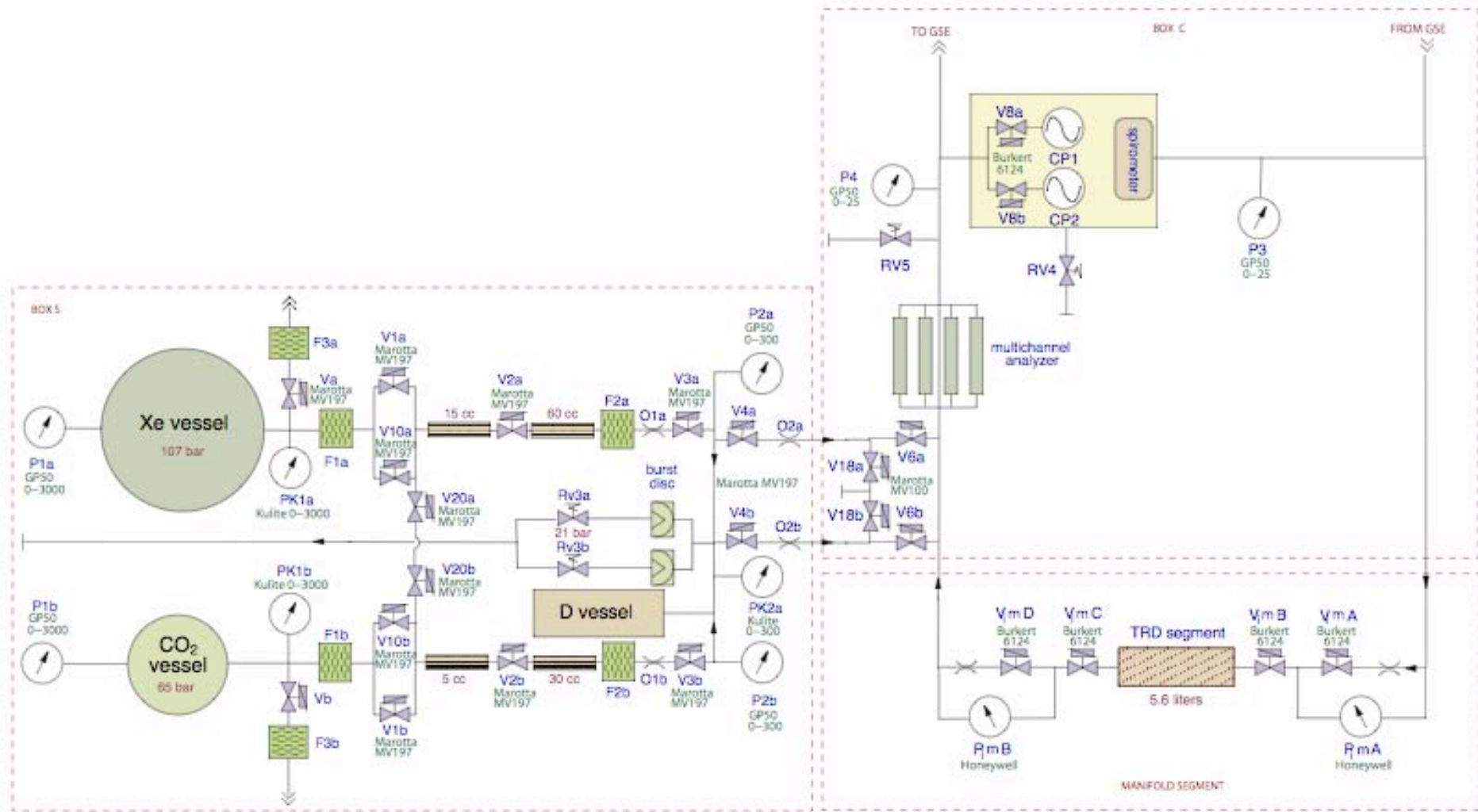
## Filling status

Ar 105 bar @ 21 °C  $V = 300\text{ml}$   $\rho = 4,3\text{mol/l}$

CO<sub>2</sub> 57 bar @ 21 °C  $V = 150,5\text{ml}$   $\rho = 9,7\text{mol/l}$

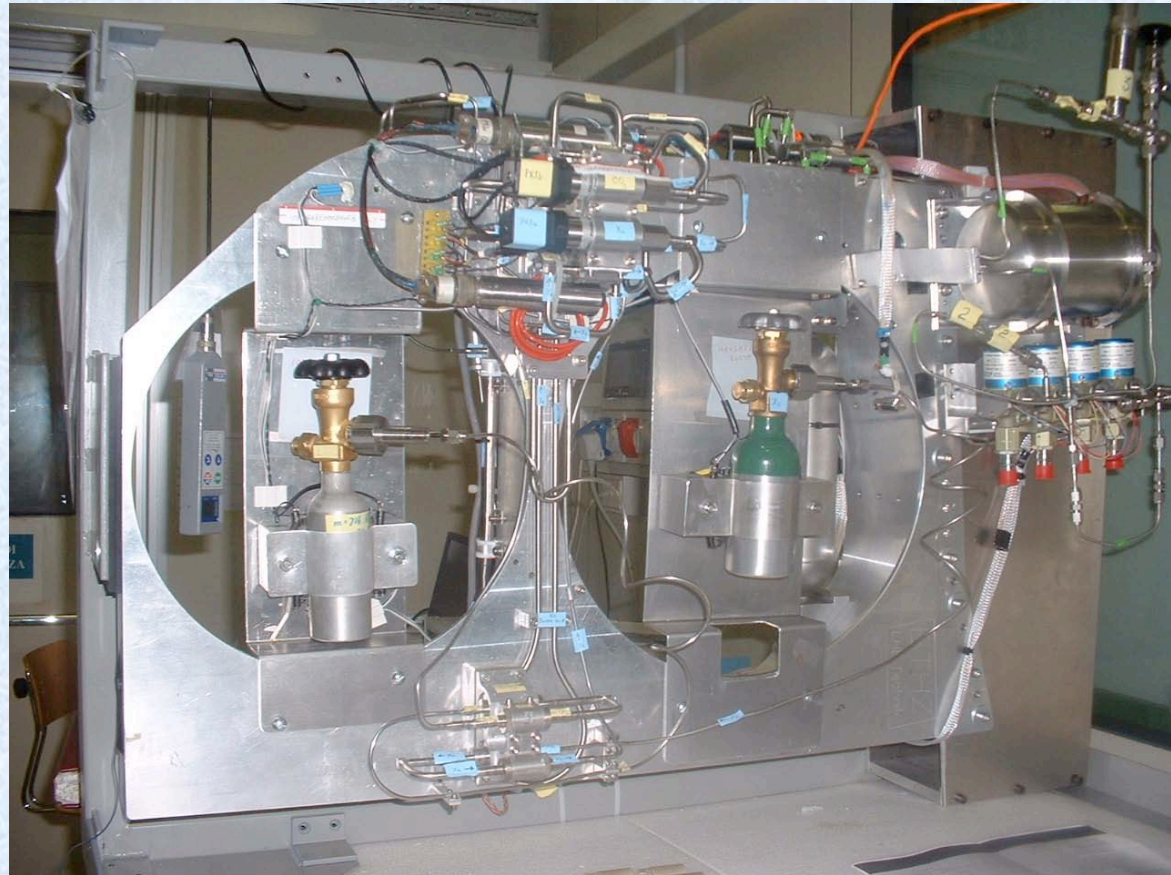


# Gas system circuit





- 9 MV197 connected (V1a, V1b, V2a, V2b, V3a, V3b, V4a, V20a, V20b)
- Heaters instead of V10a & V10b in the bottles' supports
- GP:50 P2b not connected
- 9 Dallas connected



# Test performed

- Operating valves both manually (control box) & via electronics
- Heating Ar & CO<sub>2</sub> bottles
- Dallas sensors readings
- Pressure sensors readings





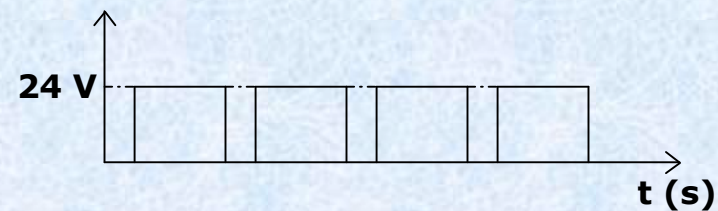
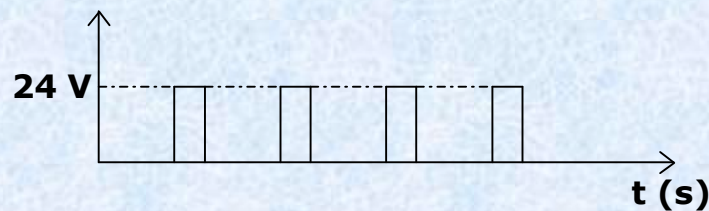
# Valves

- Operated manually & via software successfully
- Checked working status by clicks listening & leds lighting up
- V20a not working (no valve, no led): 2 pins missing on the connector
- Replaced leds on the line of V1a, V20b
- Checked the lines of disconnected stuff (V10 a&b: heaters now) by leds lighting up



# Heaters & Dallas

- Operated Ar & CO<sub>2</sub> heaters via software
- Heated Ar bottle to 24 °C changing duty from 30% to 80% (full scale 6W)



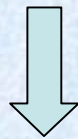
- Read out Ar Dallas to show temperature increase
- Read out all dallas successfully with increased accuracy (1/16 °C)



# Pressure sensors

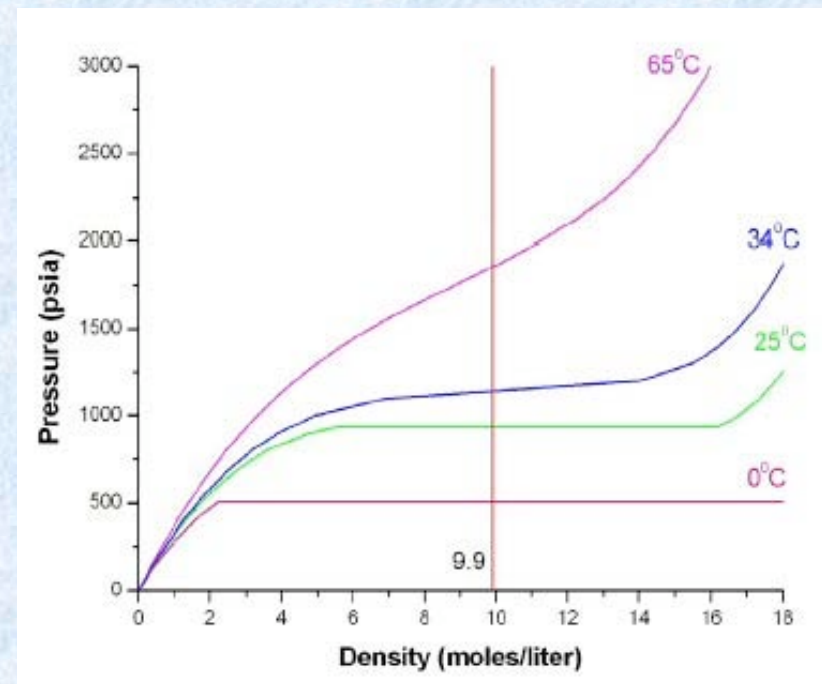
- Connected 24V & checked current
- First measurement predicted temperature

DVM: P1b ~ 1144mV = 750,17 psia



T ~ 16 °C

(NIST CO<sub>2</sub> isothermal properties)





## Discrepancy with other measurements:

clean room thermometer ~ 20 °C

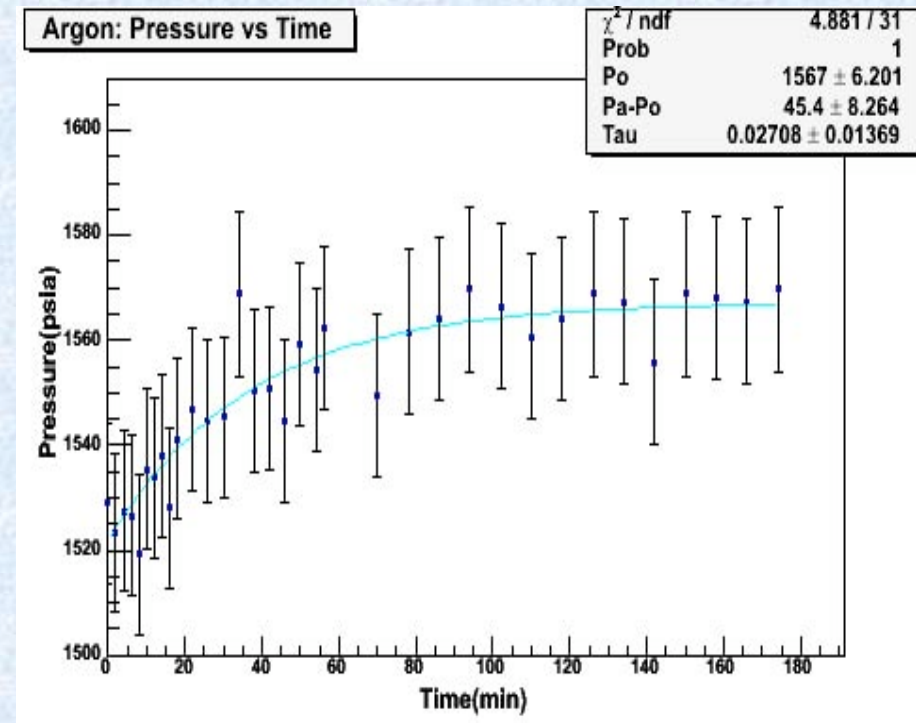
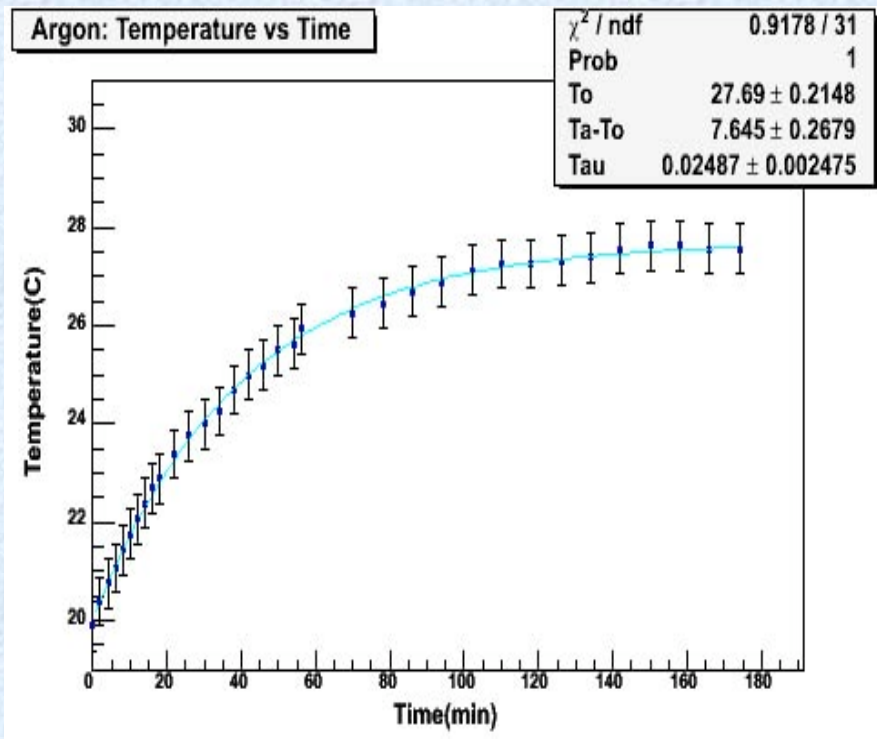
Dallas sensors ~ 20 °C

DVM probe ~ 17 °C

- Better in future (Pt thermometer)



- Ar: heated bottle at 80% duty & measured temperature and pressure

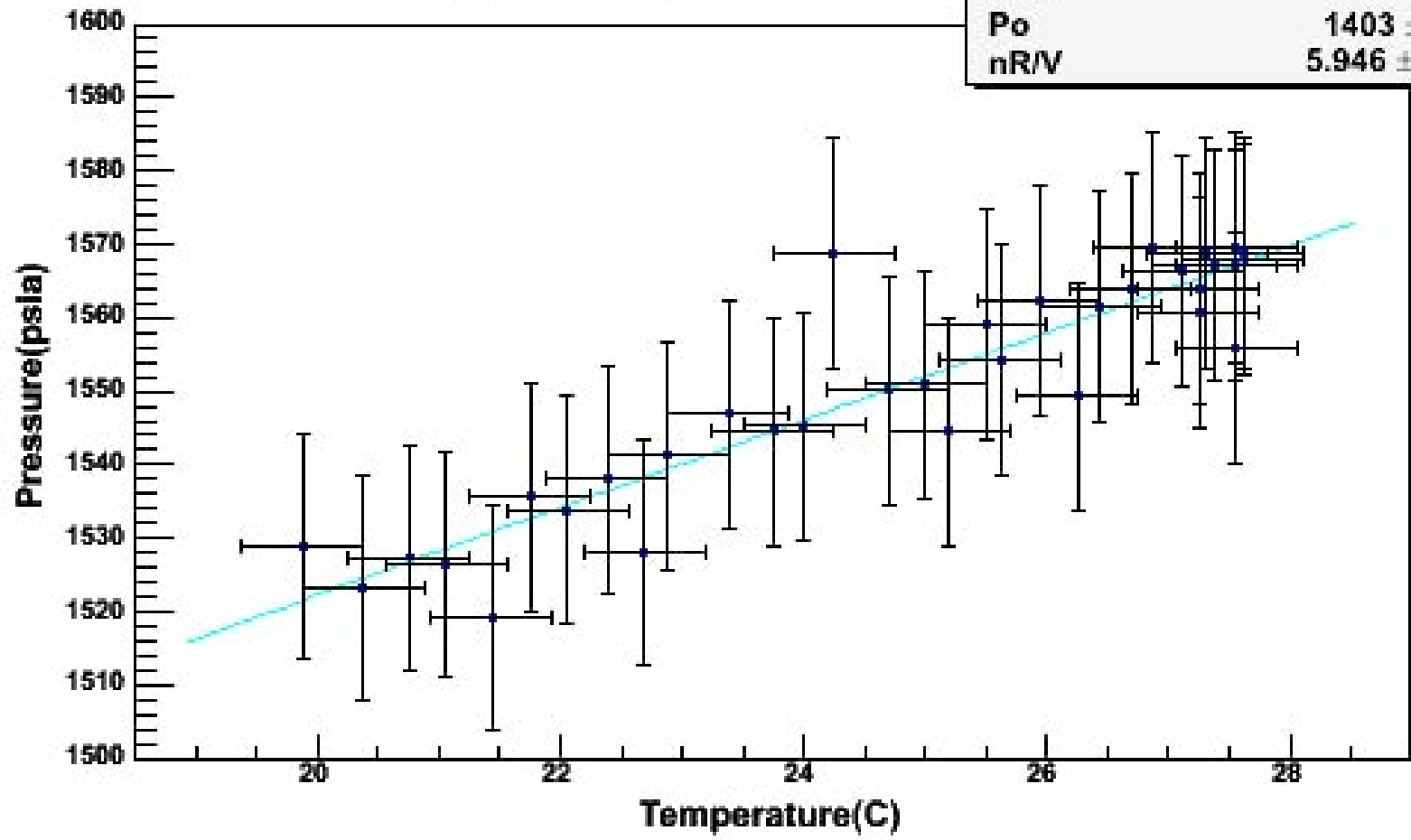


Stabilized for heat loss



### Argon: Pressure vs Temperature

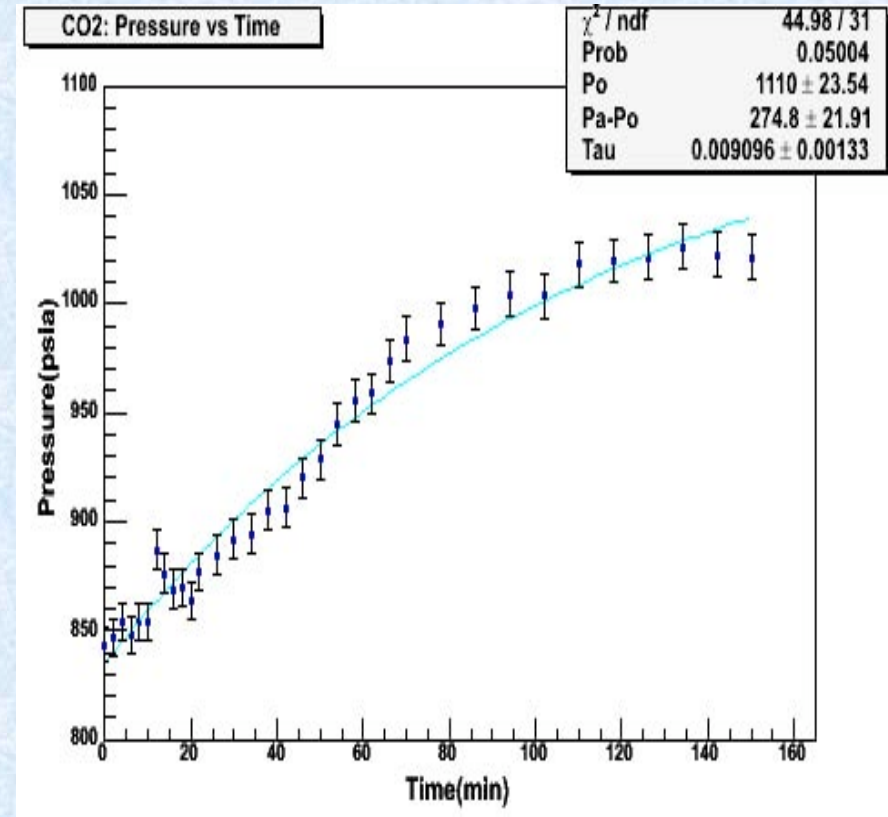
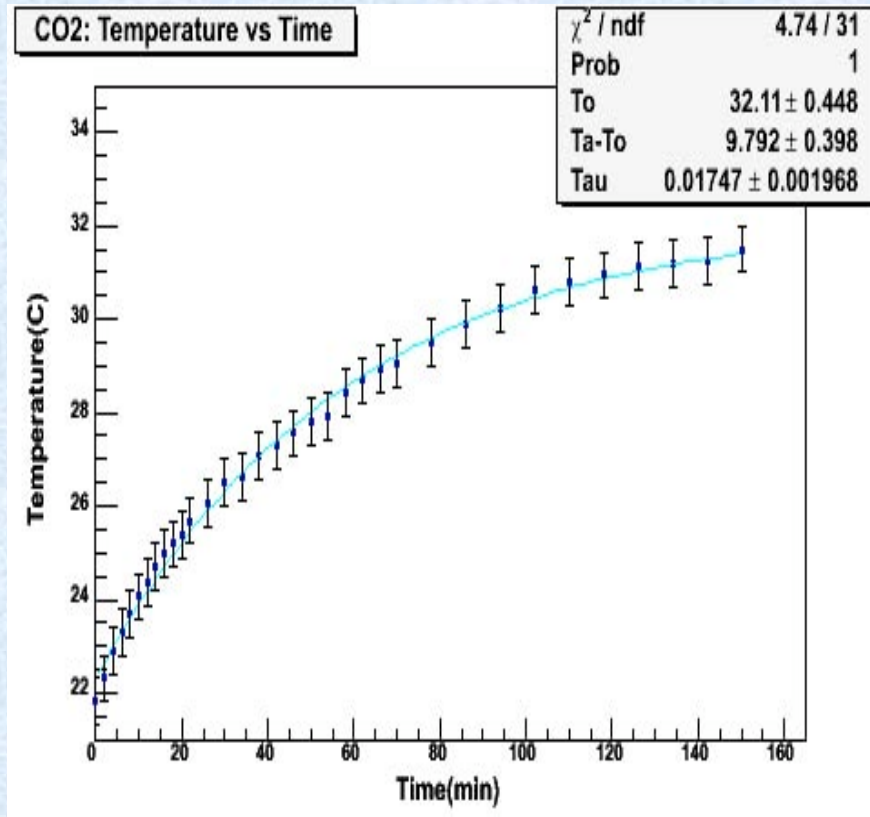
$\chi^2 / \text{ndf}$	4.931 / 32
Prob	1
Po	$1403 \pm 27.4$
nR/V	$5.946 \pm 1.102$



Ar: ideal gas



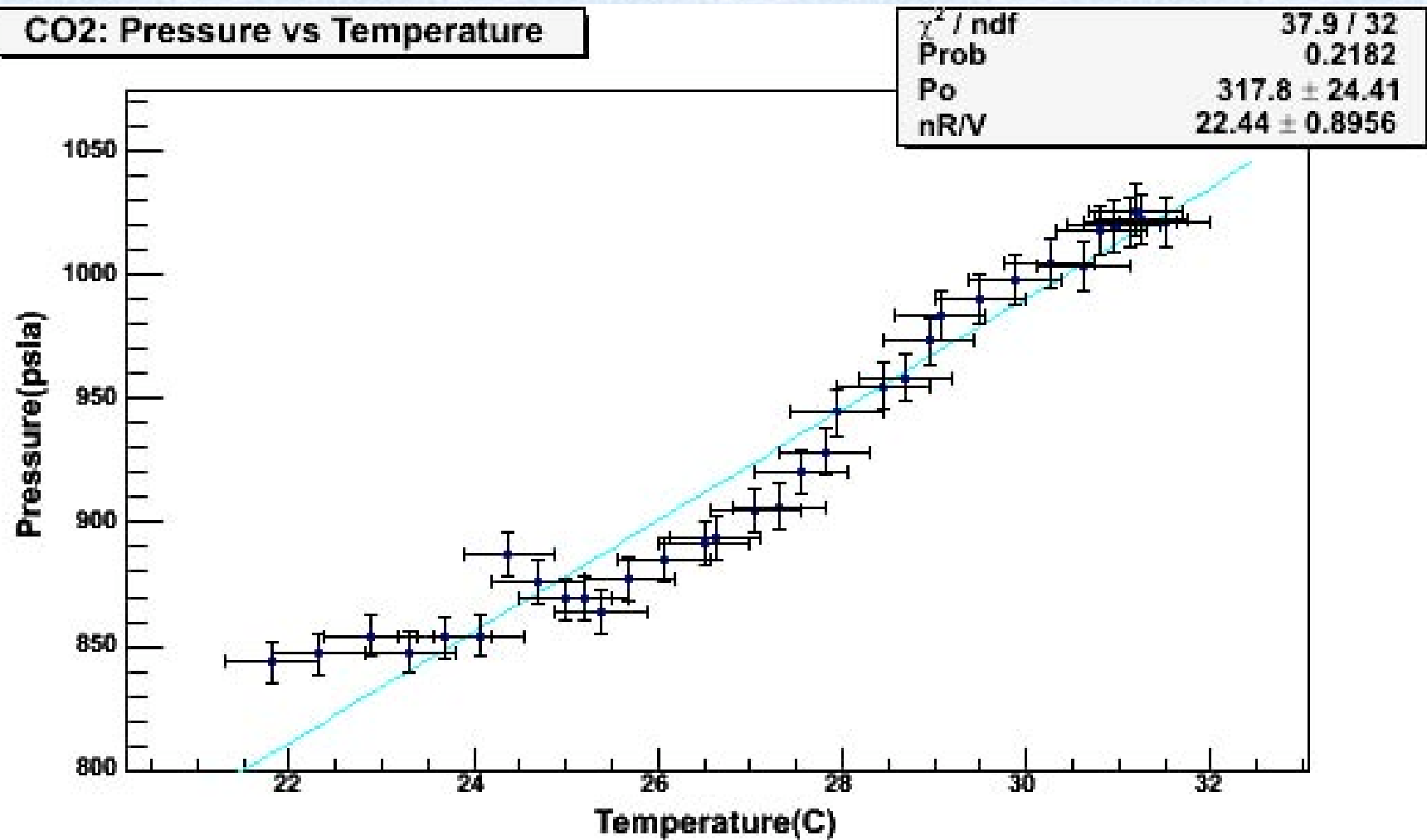
- CO<sub>2</sub>: heated bottle at 80% duty & measured temperature and pressure



Stabilized for heat loss



### CO<sub>2</sub>: Pressure vs Temperature



CO<sub>2</sub>: non ideal

# To do...

- Dallas calibration (using Pt thermometers)
- Controlling mixing procedure via software
- n shots of Ar, m shots of CO<sub>2</sub> to reach 80:20 mixture (partial pressures method)
- Operate pumps in box C
- Circulate gas through the circuit (TRD simulated by a 5l vessel)
- Spirometer reading of gases' %





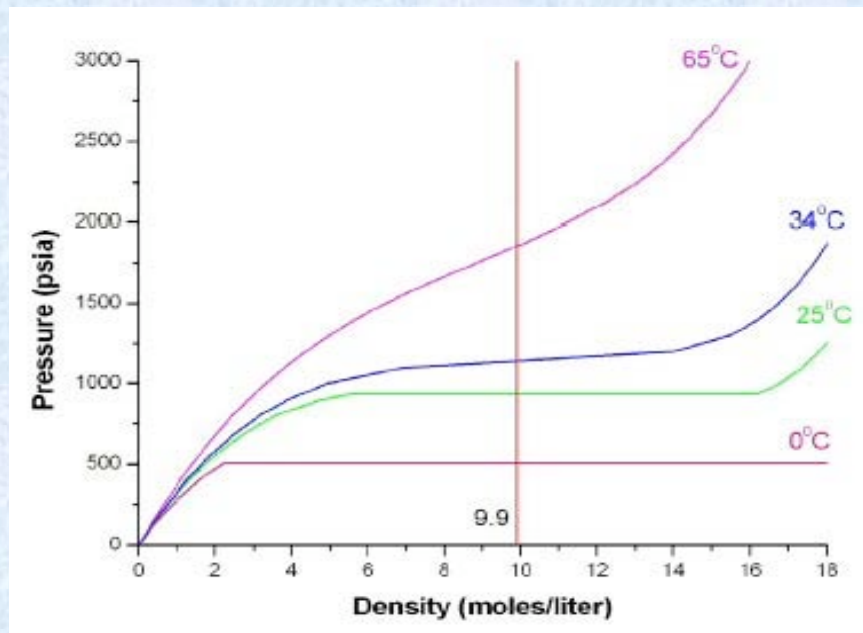
# Notes

- Most important: simulation of 1% life cycle under computer control only 10 days per cycle due to same mol/l but 1% volume
- No possibility to reach 80:20 mix exactly  
reason: bigger loss of CO<sub>2</sub> → never ideal mix.  
Adjusted mixture with the accuracy limits needed
- Calculating residual gas quantity in primary bottles  
small pressure's variation corresponding to large density variation (NIST isothermal properties) → heating needed

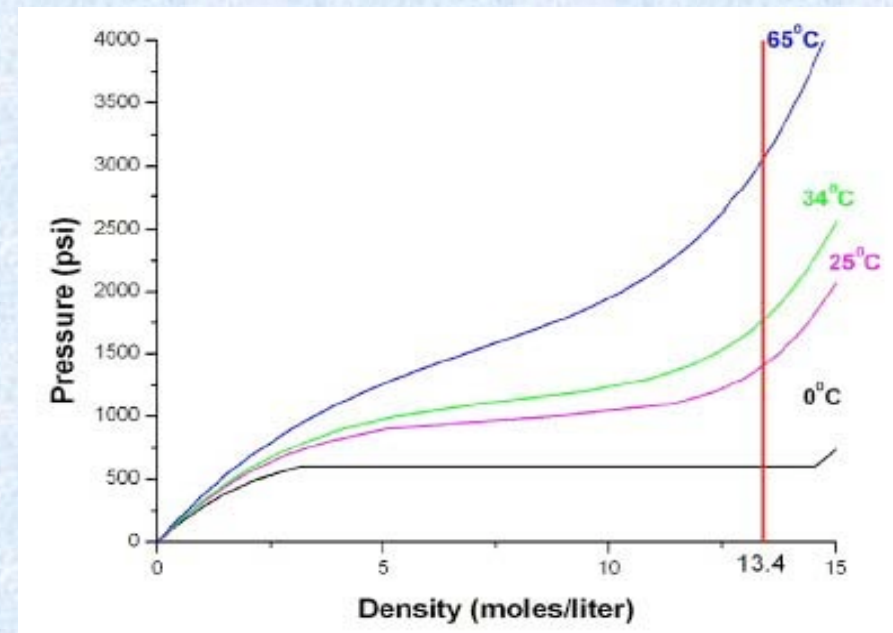


- Need to take Xe over 22°C & CO<sub>2</sub> over 34°C
- Careful temperature's readings needed  
reason: pressure increases fastly with  
temperature  $\Rightarrow$  risk of explosion

CO<sub>2</sub> isothermal properties (NIST)



Xe isothermal properties (NIST)



# Summary

- We can operate valves, T & P sensors via software
- First measurements are reasonable
- Working on box C now: pumps got running yesterday (Mariusz Sapinski & Carlo Bosio)
- Next: do 1% life cycle tests